

Catalytic NH₃ Combustion Properties of CuO_x/3Al₂O₃·2SiO₂

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Abstract: Although NH₃ has recently been regarded as a renewable and carbon-free energy source, NH₃ fuel has problems of high ignition temperature and the production of N₂O/NO_x. To overcome these problems, the present study demonstrates that the NH₃ combustion activity of copper oxide (CuO_x) catalysts supported on 3Al₂O₃·2SiO₂ (3A2S) was found to be superior to CuO_x/Al₂O₃ and CuO_x/SiO₂. The high activity for CuO_x/3A2S was closely associated with the high reducibility and small particle size of CuO_x. Finally, the relation between the local structure of CuO_x/3A2S and its catalytic NH₃ combustion properties was discussed.

Keywords: Ammonia, Catalytic combustion, Copper oxides.

1. Introduction

Recently, NH₃ has been regarded as a renewable and carbon-free energy source due to its high energy density. However, in comparison with fossil fuels, NH₃ fuel has issues including high ignition temperature and N₂O/NO_x production. Previously, we proposed novel catalytic NH₃ combustion systems that enable low ignition temperatures as well as negligible N₂O/NO_x emissions¹, and demonstrated that CuO_x/Al₂O₃ and CuO_x/SiO₂ show high activity and high N₂ selectivity for catalytic NH₃ combustion, respectively. In this study, therefore, we focused on CuO_x catalysts supported on composite oxides of Al₂O₃ and SiO₂ (3Al₂O₃·2SiO₂: 3A2S) to investigate catalytic properties for the combustion of NH₃ as an energy source.

2. Experimental

3A2S as a catalyst support material was prepared using an alkoxide method, and finally calcined at 1200 °C for 5h. Al₂O₃ (JRC-ALO-8) and SiO₂ (JRC-SIO-10) were also used as support materials for CuO_x catalysts. Supported CuO_x (6 wt% loading as CuO) was prepared by an impregnation of an aqueous solution of Cu(NO₃)₂, followed by drying and calcination at 600 °C for 3 h in air. To evaluate the thermal stability, as-prepared catalysts were thermally aged at 900 °C for 100 h in air. The catalysts were characterized by XRD, *operando* XAFS, H₂-TPR, and so on. Catalytic NH₃ combustion was conducted in a flow reactor at atmospheric pressure (10 °C·min⁻¹, 1.0% NH₃, 1.5% O₂, He balance, and W/F = 5.0 × 10⁻⁴ g·min·cm⁻³). The O₂-excess ratio on NH₃ combustion was expressed as $\lambda = (pO_2/pNH_3)_{exp.}/(pO_2/pNH_3)_{stoichiom.}$. The gas concentrations were analyzed using NDIR and gas chromatography.

3. Results and discussion

XRD patterns for CuO_x/3A2S, CuO_x/SiO₂, and CuO_x/SiO₂(aged) could be assigned to CuO and each support, whereas the diffraction peaks of Cu species for CuO_x/3A2S(aged) and CuO_x/Al₂O₃(aged) could be assigned to CuAl₂O₄. Therefore, the solid-state reaction between CuO_x and Al₂O₃ species was considered to be induced by the thermal aging at 900 °C to form CuAl₂O₄. By contrast, Al₂O₃ phase for CuO_x/Al₂O₃(aged) was partly transformed from γ to α by thermal aging. These structural results are summarized in Table 1.

Figure 1 shows Cu K-edge (a) XANES spectra and (b) FT-EXAFS for CuO_x/3A2S(aged) and CuO_x/SiO₂(aged) during NH₃ combustion ($\lambda = 2$) together with those for references. XANES spectra for CuO_x/3A2S(aged) and CuO_x/SiO₂(aged) at RT were similar to those for CuAl₂O₄ and CuO, respectively, which is consistent with the XRD patterns. However, the absorption energy of the XANES spectra for CuO_x/3A2S(aged) shifted slightly to lower energy on increasing the combustion temperature to 400 and 600 °C (see inset in Figure 1a). By contrast, the absorption energy of the spectrum for CuO_x/SiO₂(aged) at 600 °C exhibited a weak pre-edge assigned to the Cu⁺ 1s → 4p transition, which was observed in the

spectrum for Cu_2O . For FT-EXAFS (Figure. 1b), $\text{CuO}_x/3\text{A2S}(\text{aged})$ displayed an intense Cu–O peak ($r \sim 1.94 \text{ \AA}$) attributed to CuAl_2O_4 , r of which was preserved after heating at $600 \text{ }^\circ\text{C}$. These results indicate that $\text{CuO}_x/3\text{A2S}(\text{aged})$ also form CuAl_2O_4 during the NH_3 combustion. By contrast, $\text{CuO}_x/\text{SiO}_2(\text{aged})$ displayed an intense Cu–O peak ($r \sim 1.85 \text{ \AA}$) attributed to Cu_2O on reaching the reaction temperature of $400 \text{ }^\circ\text{C}$. These results are consistent with XANES and suggest that the structure of CuO in $\text{CuO}_x/\text{SiO}_2(\text{aged})$ was partly changed (reduced) to that of Cu_2O during the NH_3 combustion reaction. For $\text{CuO}_x/\text{Al}_2\text{O}_3$ before and after aging, the *operando* XAFS profiles were similar to those for $\text{CuO}_x/3\text{A2S}(\text{aged})$ (not shown here).

Table 1 summarizes the catalytic properties of supported CuO_x before and after thermal aging. T_{10} increased in the following order: $\text{CuO}_x/3\text{A2S} < \text{CuO}_x/\text{Al}_2\text{O}_3(\text{aged}) < \text{CuO}_x/\text{Al}_2\text{O}_3 < \text{CuO}_x/3\text{A2S}(\text{aged}) < \text{CuO}_x/\text{SiO}_2 \approx \text{CuO}_x/\text{SiO}_2(\text{aged})$. This finding is almost consistent with the order of the reduction temperatures observed in the H_2 -TPR experiments, suggesting that the reduction of CuO_x is closely associated with the combustion activity. In addition, it is considered that the lattice oxygen of the CuO_x surface acts as a reactant for adsorbed NH_3 , and catalytic NH_3 combustion over supported CuO_x proceeds *via* the Mars–van Krevelen mechanism. The supported CuO_x with smaller particle sizes tended to exhibit lower reduction temperatures. N_2 selectivity at T_{90} decreased in the following order: $\text{CuO}_x/3\text{A2S} \approx \text{CuO}_x/\text{SiO}_2 > \text{CuO}_x/3\text{A2S}(\text{aged}) > \text{CuO}_x/\text{SiO}_2(\text{aged}) > \text{CuO}_x/\text{Al}_2\text{O}_3 > \text{CuO}_x/\text{Al}_2\text{O}_3(\text{aged})$. Therefore, it is suggested that $\text{CuO}_x/3\text{A2S}$ before and after thermal aging exhibited improved the performance for catalytic NH_3 combustion than $\text{CuO}_x/\text{Al}_2\text{O}_3$ and $\text{CuO}_x/\text{SiO}_2$.

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4. Conclusions

During the NH_3 combustion reaction, the local structure of CuAl_2O_4 nanoparticles in $\text{CuO}_x/3\text{A2S}(\text{aged})$ was preserved, whereas that of CuO nanoparticles in $\text{CuO}_x/\text{SiO}_2(\text{aged})$ was partly changed to that of Cu_2O . The catalytic NH_3 combustion activity of supported CuO_x was closely associated with the reducibility and particle size of CuO_x , which implies that NH_3 adsorbed on CuO_x reacts primarily with the lattice oxygen. Thus, catalytic NH_3 combustion proceeds *via* the Mars–van Krevelen mechanism.

References

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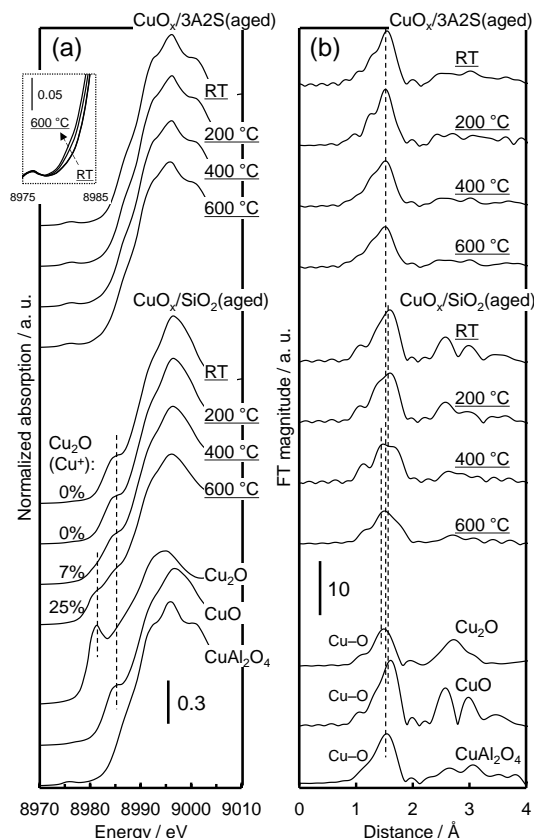


Figure 1. Cu K-edge (a) normalized XANES spectra and (b) k^3 -weighted FT-EXAFS of $\text{CuO}_x/3\text{A2S}(\text{aged})$, $\text{CuO}_x/\text{SiO}_2(\text{aged})$, and these catalysts during NH_3 combustion at reaction temperatures of 200, 400, and $600 \text{ }^\circ\text{C}$ for 30 min.

Table 1 Catalytic properties of supported CuO_x before and after thermal aging.

Catalyst	Phase	T_{10} $^a / ^\circ\text{C}$	T_{90} $^a / ^\circ\text{C}$	Selectivity at T_{90} $^a / \%$			Reduction temperature $^b / ^\circ\text{C}$	Cu particle size $^c / \text{nm}$
				N_2	N_2O	NO		
$\text{CuO}_x/3\text{A2S}$	$\text{CuO}/3\text{A2S}$	292	484	97	<1	3	209	3.1
$\text{CuO}_x/3\text{A2S}(\text{aged})$	$\text{CuAl}_2\text{O}_4/3\text{A2S}$	326	570	94	3	3	234	43
$\text{CuO}_x/\text{Al}_2\text{O}_3$	$\text{CuAl}_2\text{O}_4/\gamma\text{-Al}_2\text{O}_3$	303	476	92	6	2	185	2.4
$\text{CuO}_x/\text{Al}_2\text{O}_3(\text{aged})$	$\text{CuAl}_2\text{O}_4/\alpha, \gamma\text{-Al}_2\text{O}_3$	295	450	91	8	1	155	1.8
$\text{CuO}_x/\text{SiO}_2$	CuO/SiO_2	334	490	97	1	2	220	9.4
$\text{CuO}_x/\text{SiO}_2(\text{aged})$	CuO/SiO_2	335	557	93	4	3	234	17

a Temperature at which NH_3 conversion reached 10% and 90%. b Temperature of the first H_2 consumption peak determined by H_2 -TPR. c Calculated from H_2 -TPR after H_2 reduction and subsequent N_2O reoxidation.