

# (EtOH+NH<sub>3</sub>) synergism in lean-NO<sub>x</sub> reduction over Ag/Al<sub>2</sub>O<sub>3</sub> catalyst

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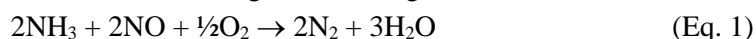
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**Abstract:** The implemented Urea-SCR technology is an effective process for NO<sub>x</sub> reduction from Diesel vehicles but is strongly dependent at low temperature (175-250°C) to the NO<sub>2</sub>/NO<sub>x</sub> ratio. By means of co-feeding of ammonia and ethanol over Ag/Al<sub>2</sub>O<sub>3</sub> catalyst, a drastic enhancement of the NO<sub>x</sub> conversion is evidenced using only NO as NO<sub>x</sub>. The ammonia activation is mainly attributed to the availability of hydrogen H\* species resulting from EtOH oxidation. A remarkable DeNO<sub>x</sub> efficiency is additionally achieved with a dual-bed configuration (Ag/Al<sub>2</sub>O<sub>3</sub>+NH<sub>3</sub>-SCR catalyst) leading to impressive performances of this EtOH-assisted process without critical dependence to the NO<sub>2</sub> yield.

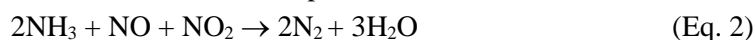
**Keywords:** SCR, DeNO<sub>x</sub>, Ag/Al<sub>2</sub>O<sub>3</sub>.

## 1. Introduction

Reduction of NO<sub>x</sub> compounds from Diesel and lean burn engine remains a major challenge at low temperature. The selective catalytic reduction (SCR) of NO<sub>x</sub> by urea/NH<sub>3</sub> is well established and used worldwide to convert NO<sub>x</sub> into nitrogen, according to the so-called standard-SCR reaction (Eq. 1)<sup>1</sup>:



However, in this condition, the activity at low temperatures (175-250°C) remains limited and improvement requires prior oxidation of NO to NO<sub>2</sub> to promote the more favorable fast-SCR reaction (Eq. 2):



NO<sub>2</sub> yield can be adjusted by the Diesel oxidation catalyst (DOC) upstream the SCR converter. In practice, the NO<sub>2</sub>/NO<sub>x</sub> ratio depends on the DOC activity, which also undergoes kinetic limitation at low temperature and penalizes the deNO<sub>x</sub> efficiency of the SCR converter downstream.

EtOH-SCR process was also described as an attractive way to reduce NO<sub>x</sub> with silver-based catalysts<sup>2</sup>. The NO conversion is assumed to be strongly dependent of the nitromethane route formation, based on the ethanol oxidation to acetaldehyde *via* a variety of intermediates which are subsequently adsorbed as surface acetate and ethoxide ions. N-containing compounds such as HNCO and ammonia are also involved in the NO<sub>x</sub> reduction mechanism<sup>3</sup>. Unfortunately, this system also suffers from limited activity at low temperature, although partial oxidation of ethanol leads to high NO<sub>2</sub> emission in the 175-300°C temperature range<sup>4</sup>.

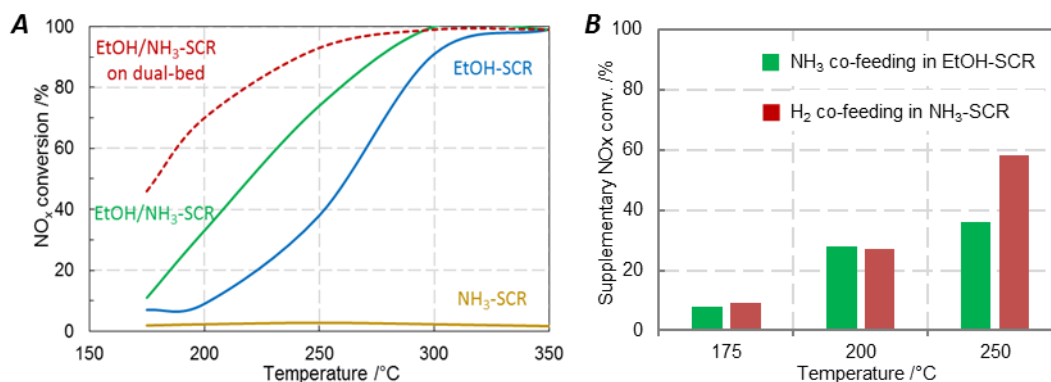
This work aims to demonstrate the beneficial co-feeding of ethanol and ammonia (EtOH/NH<sub>3</sub>-SCR) over Ag/Al<sub>2</sub>O<sub>3</sub> to enhance the low temperature NO<sub>x</sub> reduction in the unfavorable standard-SCR condition.

## 2. Experimental

2% Ag/Al<sub>2</sub>O<sub>3</sub> (Ag/Al) and WO<sub>3</sub>/Ce<sub>x</sub>Zr<sub>1-x</sub>O<sub>2</sub> (WO<sub>3</sub>/Ce-Zr) catalysts were prepared according to ref 5. Catalytic tests were performed in a quartz tubular micro-reactor under a synthetic flow containing or not 1200ppm EtOH, with or without 400ppm NH<sub>3</sub>, 400ppm NO, 8% H<sub>2</sub>O, 10% CO<sub>2</sub>, 10% O<sub>2</sub>, N<sub>2</sub>. Three reductants were evaluated, namely ethanol (EtOH), NH<sub>3</sub>, and a blend (EtOH+NH<sub>3</sub>). Gaseous NO/NO<sub>2</sub>/NH<sub>3</sub>/O<sub>2</sub>/N<sub>2</sub> gas flows were adjusted by mass-flow controllers (Bronkhorst). Ethanol aqueous solution (8.02 10<sup>-1</sup> mol L<sup>-1</sup>) was vaporized and mixed upstream the SCR catalyst by means of a micro-nozzles provided by The Lee Company (Ø<sub>nozzle</sub>= 50 µm) connected to a HPLC pump (Jasco, PU-2085, 22 µL min<sup>-1</sup>, ΔP=10 Bar). The compositions of the feed gas and effluent stream were monitored continuously using online MKS 2030 Multigas infrared analyser for NO, NO<sub>2</sub>, N<sub>2</sub>O, HNCO, NH<sub>3</sub>, CH<sub>3</sub>CH<sub>2</sub>OH, CH<sub>3</sub>CHO, CH<sub>3</sub>OH, CH<sub>2</sub>O, C<sub>2</sub>H<sub>4</sub>, CH<sub>4</sub>, CO, CO<sub>2</sub> and H<sub>2</sub>O.

### 3. Results and discussion

The effect of reducers ( $\text{NH}_3$ , EtOH and EtOH/ $\text{NH}_3$ ) on  $\text{NO}_x$  conversion over Ag/Al catalyst (full line) is reported in Figure 1A. With ethanol as reductant (EtOH-SCR),  $\text{NO}_x$  conversion was 9% and 38% at 200 and 250°C, respectively (blue curve). When ammonia was co-fed in the mixture, an important gain was denoted (green curve). The  $\text{NO}_x$  conversion reached 33% and 74% at 200°C and 250°C, respectively. No significant  $\text{NO}_x$  conversion was recorded with only ammonia whatever the temperature (yellow curve), which means that the ammonia activation is due to the presence of ethanol over Ag/Al sample.



**Figure 1.** (A): Effect of the reducers used on the  $\text{NO}_x$  conversion profile over Ag/Al (full line) or a dual-bed system Ag/Al+ $\text{WO}_3$ /Ce-Zr (dotted line); (B): Comparison of  $\text{H}_2$  addition in  $\text{NH}_3$ -SCR and  $\text{NH}_3$  addition in EtOH-SCR over Ag/Al.

As reported in Figure 1B, this EtOH+ $\text{NH}_3$  synergistic effect is mainly attributed to the ethanol dehydrogenation leading to the formation of surface hydrogen  $\text{H}^*$  ad-species allowing a mechanism related to  $\text{H}_2$  assisted  $\text{NH}_3$ -SCR process over Ag/Al catalysts<sup>6</sup>. Our hypothesis, supported by the characterization of adsorbed species followed by FTIR, is that these  $\text{H}^*$  species are involved in  $\text{HNO}_x$  species, which are known to be very reactive with  $\text{NH}_3$ <sup>7</sup>.

However, in this EtOH/ $\text{NH}_3$ -SCR process over Ag/Al, unconverted  $\text{NH}_3$  and  $\text{NO}_x$  remained. To further improve the  $\text{NO}_x$  conversion, experiments were carried out adding a conventional tungsten based  $\text{NH}_3$ -SCR catalyst downstream to Ag/Al sample. In this dual-bed system, the  $\text{NO}_x$  conversion profile (Figure 1, red dotted line) exhibited a supplementary significant improvement. The  $\text{NO}_x$  conversion varied from 46 to 95% in the 175-250°C temperature range. This high activity is due to a supplementary conversion occurring on the  $\text{NH}_3$ -SCR catalyst, via the fast-SCR reaction.

### 4. Conclusions

The  $\text{NH}_3$ -EtOH-SCR process over Ag/Al catalyst was evidenced to significantly improve the  $\text{NO}_x$  reduction at low temperature in the unfavorable standard SCR condition. The formation of  $\text{H}^*$  species (from ethanol oxidation) is proposed to promote the  $\text{NH}_3$ -SCR over Ag/Al<sub>2</sub>O<sub>3</sub>. Moreover,  $\text{NO}_2$  (from  $\text{NO}$ +EtOH reaction) can be used in a dual-bed coupled system composed of Ag/Al and a conventional  $\text{NH}_3$ -SCR catalyst to supplementary improve the  $\text{NO}_x$  reduction by  $\text{NH}_3$ . A remarkable enhancement of the de $\text{NO}_x$  efficiency was achieved without dependence to the activity of the upstream oxidation catalyst (DOC). It makes this process an attractive way to increase the crucial low temperature SCR activity in  $\text{NO}$ -rich media and offer promising new avenue to achieve the future stringent regulations of lean-burn passenger cars.

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